2nd World Congress on Petroleum and Refinery



Experiment Studies on N₂ - viscosity Depressant with Steam Stimulation for Shallow Thin Superheavy Oil Reservoirs

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China University of Petroleum

2.6.2017 Osaka

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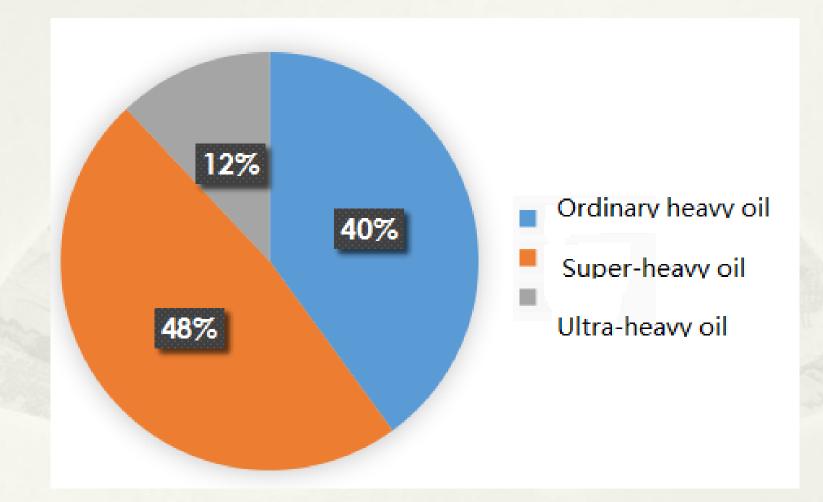


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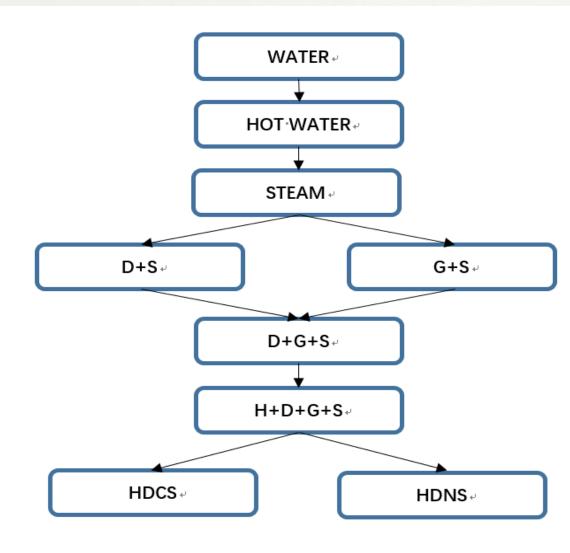
Table 1 Classification of heavy oils

Туре		Viscosity(cp)	Specific Gravity
Ordinary heavy oil	1	50-150	>0.92
	2	150-10000	>0.92
Super-heavy oil		10000-50000	>0.95
Ultra-heavy oil		>50000	>0.98

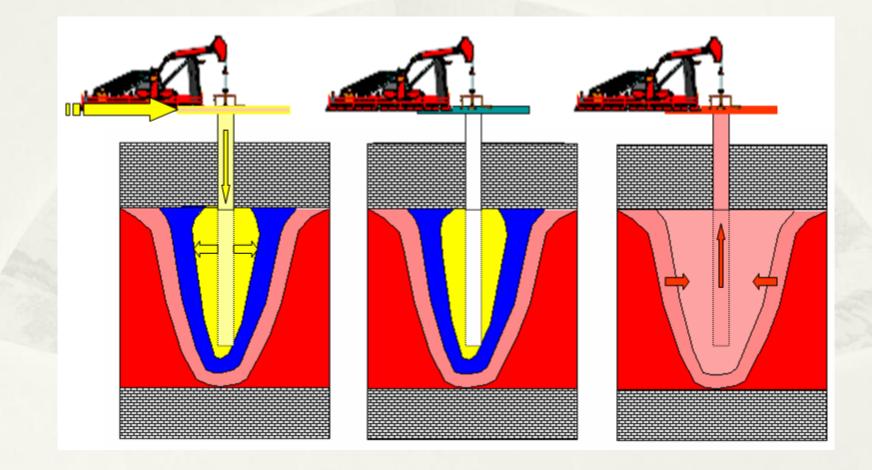


Methods:

- (1). Steam stimulation
- (2). Steam flooding
- (3). Combustion in-situ
- (4). Hot water flooding
- (5). Electromagnetic heating



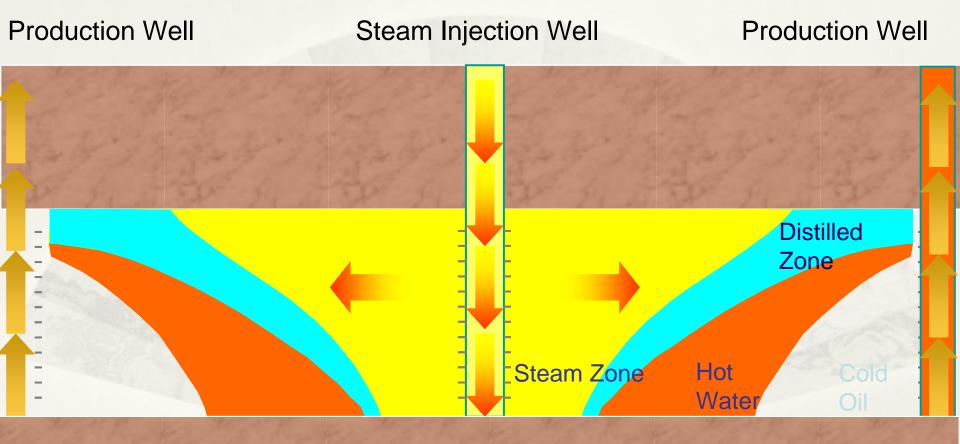
Steam huff and puff



Cyclic steam injection, steam soak, steam huff and puff

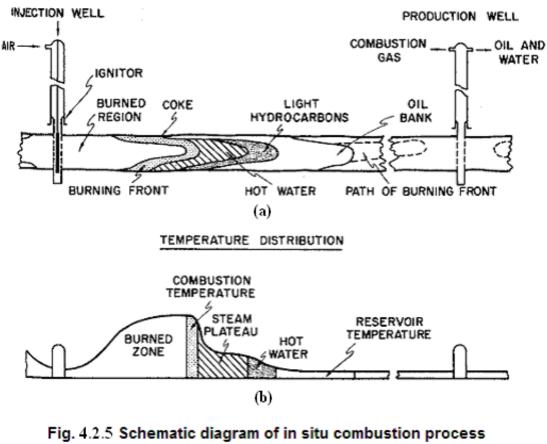
Mechanism:

(1) Thermal expansion of fluids
 (2) Compression of solution gas
 (3) Reduced residual oil saturation
 (4) Wellbore cleanup effect



Steam Flooding

In-situ combustion



(modified from Nelson and McNcil, 1961)

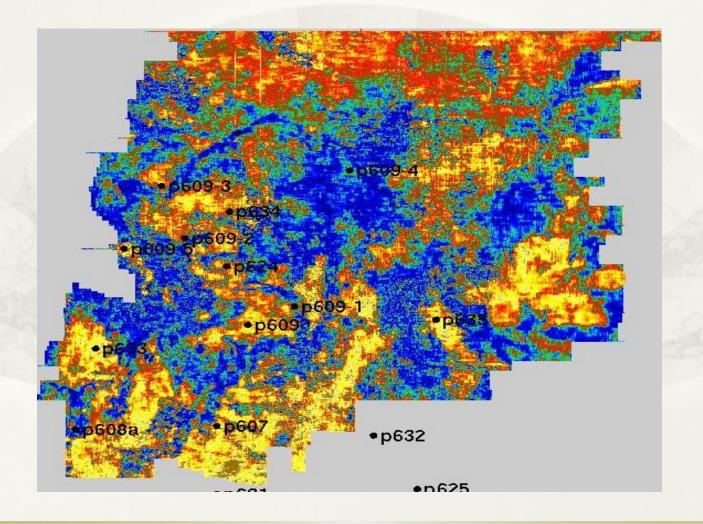
Classifications of gas injection:

(1) Miscible displacement
 (2) Near-miscible displacement
 (3) Immiscible displacement

Gas used:

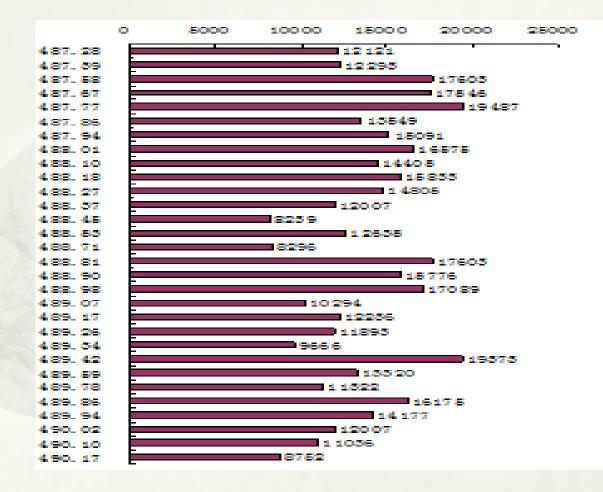
(1) CO₂
(2) N₂
(3) air

The typical Oil Field



Characteristics of the heavy oil reservoir:

Shallow: the reservoir Depth 400-700m Thin: The reservoir thickness 2-8m Low temperature: 30°C Low pressure: The reservoir pressure <5.0MPa Viscous: Oil viscosity 50000-90000mPa·s @ reservoir temperature



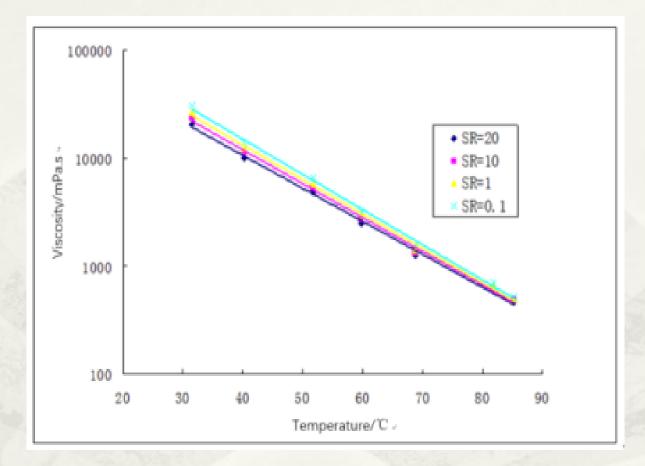
Vertical distribution of permeability

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2 Experimental



The relationship between viscosity and temperature of the oil sample

2 Experimental

2.1 Materials

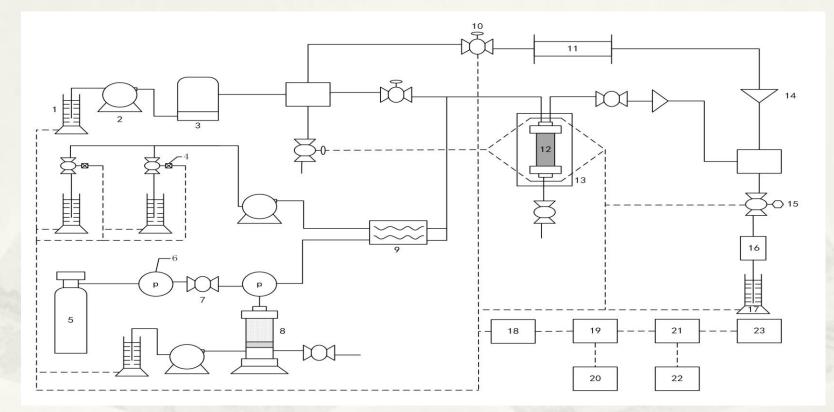
Crude oil; Simulated Water (35000mg/L, KCl); YR-2 Oil soluble viscosity reducer; Nitrogen; Sand filled models

basic parameters of sand filled models

No.	L/cm	D /cm	ф /%	K /μm²	No.	L/cm	D /cm	ф/%	K /μm²
1	18	3.83	34.82	3.15	9	18	3.83	35.46	3.18
2	18	3.83	35.19	3.23	10	18	3.83	36.04	3.26
3	18	3.83	35.14	3.07	11	18	3.83	35.22	3.21
4	18	3.83	35.23	3.16	12	18	3.83	36.43	3.35
5	18	3.83	34.95	3.23	13	18	3.83	36.18	3.32
6	18	3.83	36.36	3.21	14	18	3.83	34.88	3.02
7	18	3.83	35.78	3.35	15	18	3.83	35.54	3.19
8	18	3.83	34.92	2.99					

2 Experimental

2.2 Equipment



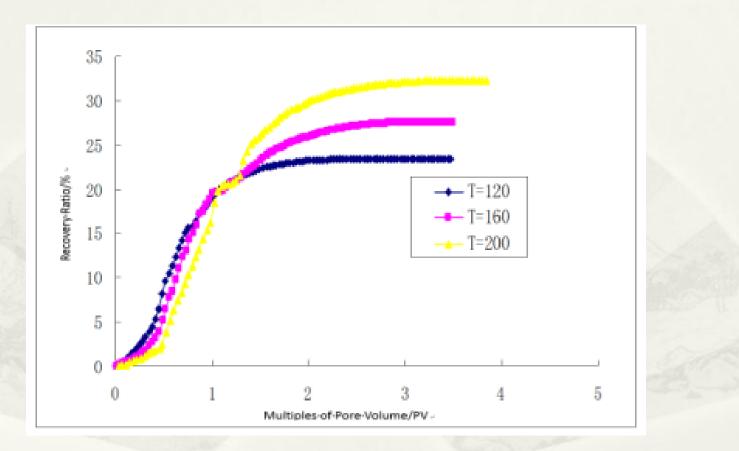
aquamanile 2.pump 3. Steam generator 4. Solenoid valve 5. nitrogen vessel 6. pressure gauge 7. Valve
 intermediate vessel 9. heat preservation jacket 10. electromotive valve 11. Damper 12. Sand Pack
 Thermostatic Box 14. check valve 15. Pressure regulating valves 16. oil-water separator 17. electronic balance
 Intermediate coefficient 19. Acquisition date20. Console 21. microcomputer data processing and control system
 Printer 23. Graph-Plotter

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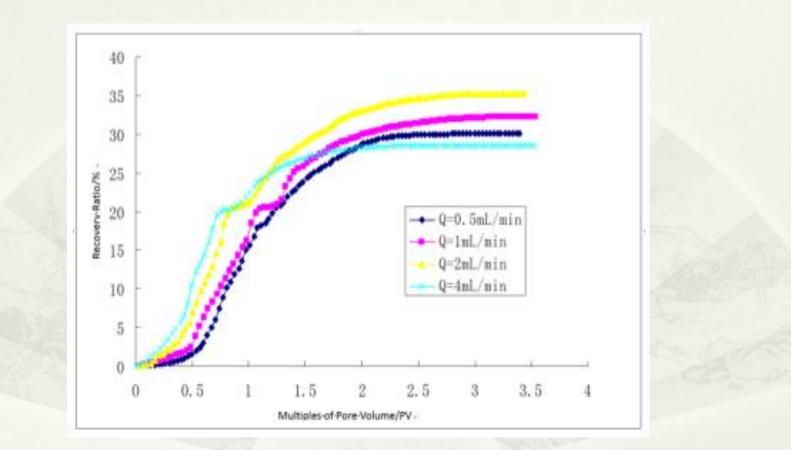
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3.1 Effect of Steam Temperature



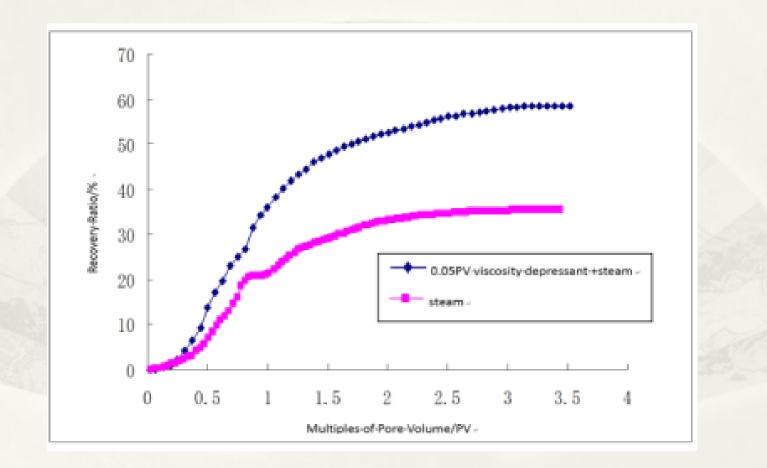
The relationship of recovery ratio with injected pore volume for different steam temperature

3.2 Effect of Steam Injection Rate



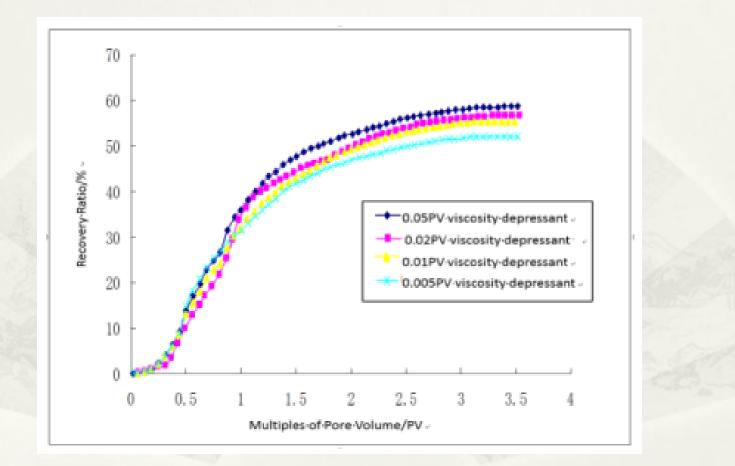
The relationship of recovery ratio with injected pore volume for different steam injection rate

3.3 Effect of Viscosity Depressant



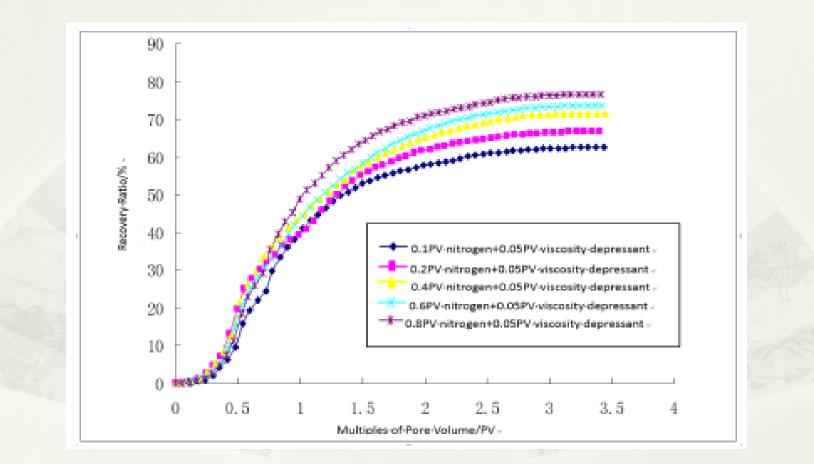
The relationship of recovery ratio with injected pore volume for D+S

3.4 Effect of injected volume of viscosity depressant



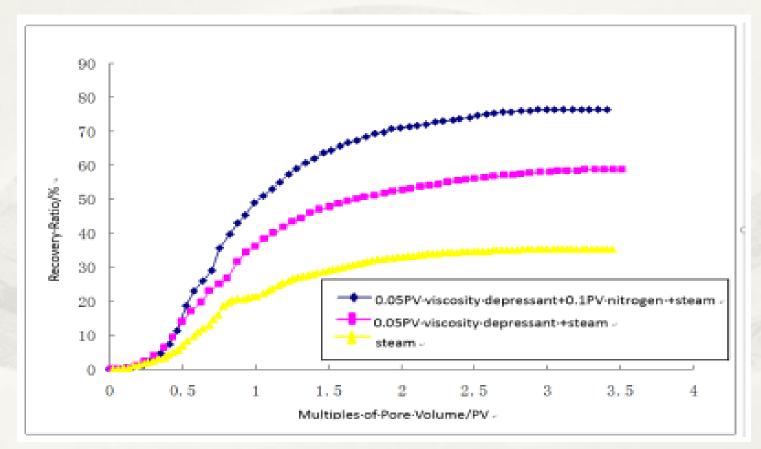
The relationship of recovery ratio with injected pore volume for different volume of viscosity depressant

3.5 Effect of Nitrogen

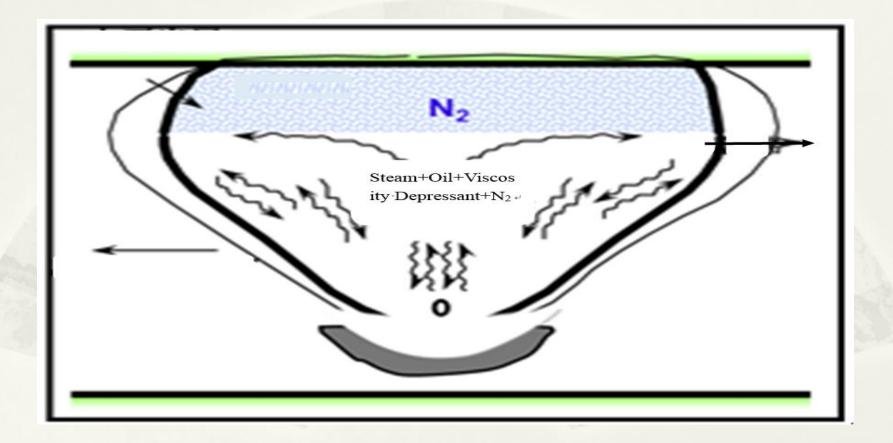


The relationship of recovery ratio with injected pore volume for different amount of nitrogen

3.6 Comparison of Different Recovery with Different Flooding Methods



The relationship of recovery ratio with injected pore volume for different flooding methods



Mechanism of HDNS

(1) The function of heat insulation and preservation: the nitrogen thermal conductivity is lower than oil, water and rock. It conducts heat slowly into the formation, reducing heat loss. And nitrogen gas can be accumulated in the top of the reservoir, suppressing the steam over-reduced heat loss, improve thermal efficiency.

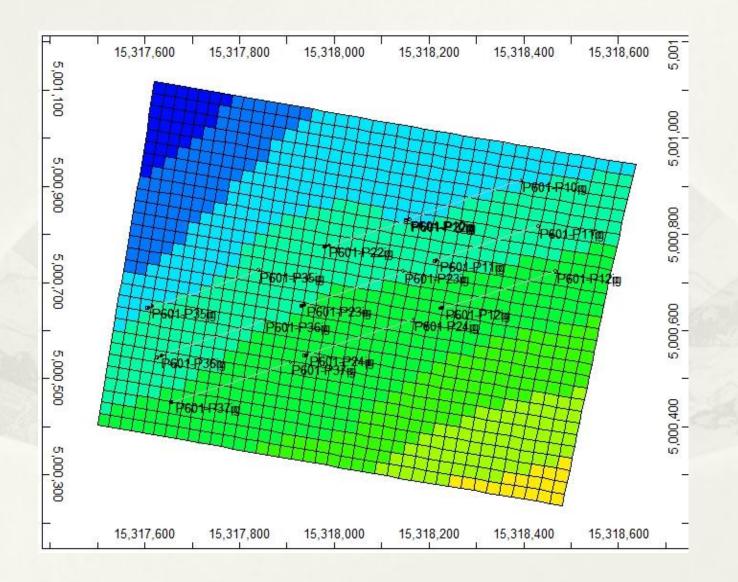
(2) Increasing energy: under the same conditions, nitrogen provides elastic energy is 1.25 ~ 1.5 times as that of carbon dioxide gas, so the nitrogen can increase the pressure.

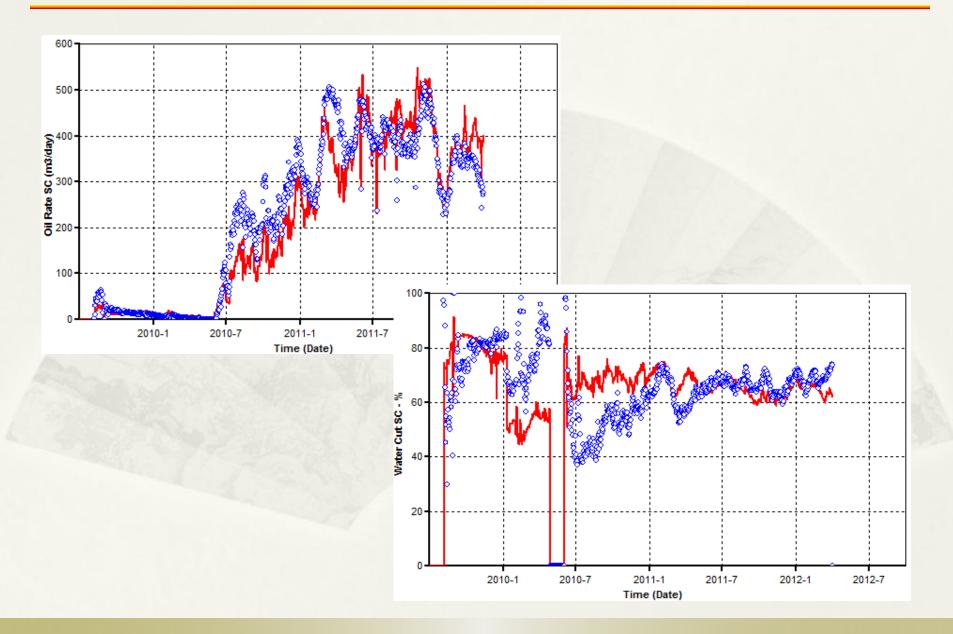
(3) Reducing viscosity: oil-soluble viscosity reducer can break down gum and asphaltenecan, forming a dispersion system in which the colloidal asphaltene is a dispersed phase and the crude light component is a continuous phase. And viscosity reducer can improve the flow condition, which is conducive to enhancing oil recovery. Moreover, the synergistic effect of viscosity reducer and nitrogen can further expand the radius of viscosity.

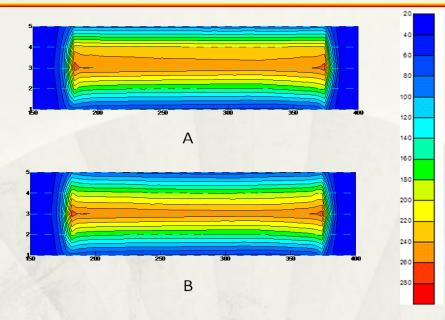
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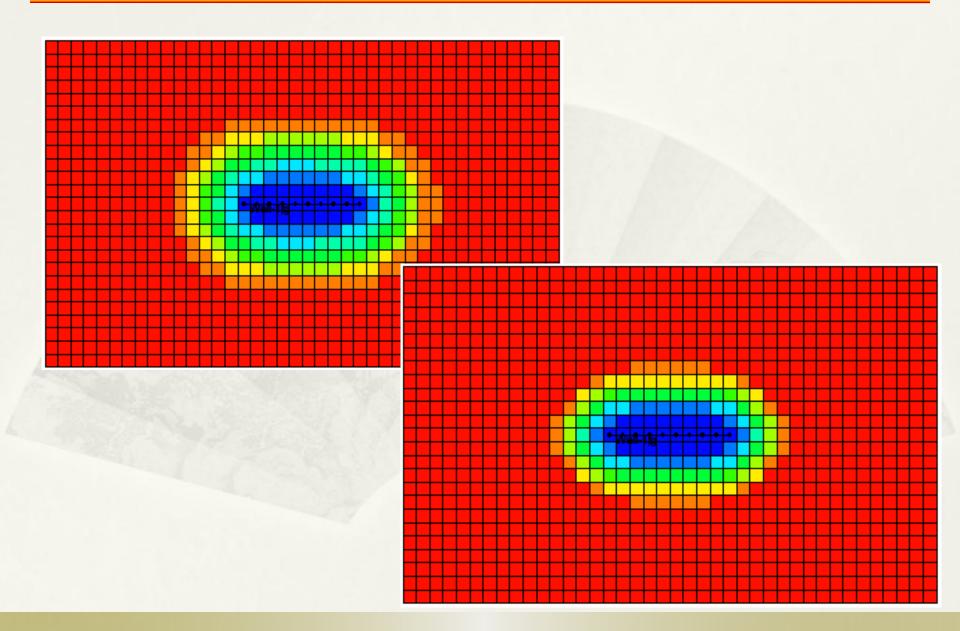
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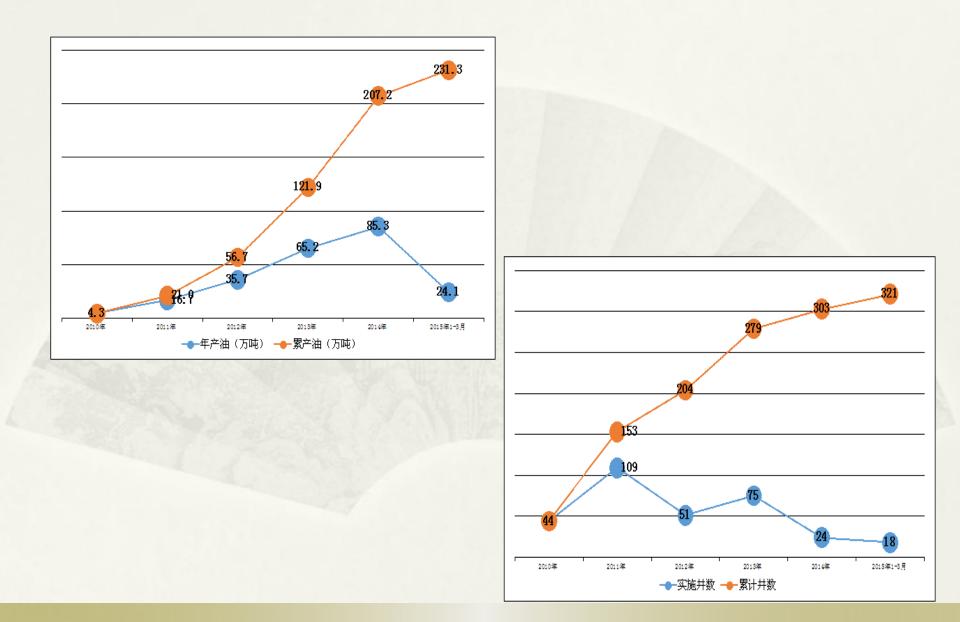
S+D

S+N

HDNS

7317 59.1 °C	5008 62.1 T	1315 14,7 °C	242.80	7505 73.8°C	tanz 60. 4 T	1311 57. 1°C		7368 72.1 °C	1315 124, 4 ¹ 0	1314 234.10	1303 125. 00	1312 10. 4 TC	1311 ST. 1 ⁹ C	59.1 °C	62.1 T	1505 107.7 °C	1314 235. SC	1313 109. 9 0	1502 00.4 °C	57.17C	731Y 00.2 T	93.1 °C	131.2 T	1314 224. 90	536.20 536.20	1312 94.2 T	1311 50. 17
45-	7205	7355		733_	T322	T321	- 45-	1200	185 an		1782	1322	Helen -	45-	7205 59.4 T	Ties	1224	T223	T102	1221	45-	7305	135		7323	1302	
40-	54 4 C	#7 C		1.40	M.TC	SEEC	- 40-	012 0	115.0 0		in the	10.1 G		40-		105.5 C				64.6C	40-	94.3 °C	121.90	218.40	12.4	W.FC	61.2C -
35- 55.0 °C	7336 57.5 °C	7335 70.612	7334 219.90	7335 T0.010	7332 54.6 °C	53. 9°C	- 35-	1336 67.1 %	1306 110. 4 7	1334 217.70	7333 112, 85	T332 66.6 T	T331 53. 9/C	35- 1337 95.0 %	1336 51.5 °C	1385 104.33	1334 220. 90	1333 108. ft;	7332 54.6 °C	1331 53.970	35- 55.6 to	7306 87.7 °C	7335 120. C	7304 209. 30	7333 122.60	7302 88.1 °C	T201 56. 1°C
30-							- 30-							30-							30-						
25- ¹³⁴⁷ 55.0 ¹⁷	7346 55.5 °C	7945 97.270	7344 212.40	7543 T0.07C	24CT 27.9.10	7343 53. TC	- 25 - ⁵³⁴⁷	7345 65.9 °C	1345 105.4C	7344 205 / fC	7343 109. 80	1942 60.270	тэн 53.11С	25- ⁵³⁰	7348 55.5 °C	7945 101. 1 0	7344 210.42	1343 134.20	1342 54.910	1341 53.7°C	- 25- ^{53/7} 55.0 T	7346 85.2 °C	1345 115.80	T344 199. 30	1940 112.40	T942 88.2 °C	тэч. 5т. 2°С —
20-							- 20-							20-				-			20-				-		
54.20	95.2 °C	376.38	206.30	63.170	53.7 °C	55. TC	- 15-	05.8 V	105. C	192.92	106. đC	67.170	55. TC	54.2°C	7796 55.2 °C	96.90	202.17	501.7C	\$3.7 °C	55.7°C	15-	85.6 °C	in.sc	193. ØC	109. đC	67.1 °C	26.30
10- T30T	7386 56 4 m	T365	7354	T363	T362	T361	- 10-	2364	T265	1394	7363 1995 da	1362	T261	10-	58.4 °C	T365	724	7353	T362	7361	10-	1364	1325	T264	7363	T362	T261
5-			- Marie				- 5-	21.6						5-				30.46			- 5-			and the			-
0-THT 98.1 TC	7376 58.0 °C	7315 57.170	1374 197.80	7575 60.170	тэте 58.4°С	17571 571-382	711.00 0 1.00	7378 65.0 °C	T315 101.00	1374 196.80	7373 102. 3 0	7372 66.2 °C	1311 56. 1°C	D 1.00	1276 50.0 °C	7315 25.32	1374 195. 82	1373 96.5°C	1312 56.4°C	1371 56.1°C	1377 54.1 °C	1316 75.5 °C	1375 105. \$2	T374 107. 00	1373 139. TC	T372 76.2 °C	7371 53. 2°C
Ó	5 10	15 20	25	30 35	5 40	45	0	5 10	15 20	25	30 35	40	45	Ö	5 10	15 20	25	30 35	40	45	0 5	10	15 20	25	30 35	40	45





应用证明

	200							
项目名称	薄浅层菇	稿油油藏高效开发关键技术研究与应用						
应用单位	中国石油化工程份有限公司胜利油田分公司新春采油厂							
通讯线社	山东东营市西国路 633 号胜建大厦新春采油厂, 257000							
应用成果起止时间	2014.4-2014.06							
	经济外	故益(万元)						
年度	2014							
新培产值(产量)	63							
新堆利税(纯收入)	21							
年增收节支总额	7							

阿拉德油田位于准噶尔盆地北缘,哈线 22 块位于该油田东部,油藏埋深 570m 左右, 镇层厚度 7m, 含油面积 2.5km², 50℃脱气原油黏度 5720 mPa·s. 哈线 22 并采用蒸汽吞吐辅助氯气技术试采三个周期,峰值日产油 3~6t/d. 周期生产天数 36~121 天,周期产油 174~425t,周期油汽比 0.15~0.22,回 采水率 10%~52%。

为改善开发效果, 部署了1口水平井(哈波 22-平1井), 水平段长度 230 米, 采用 HDNS 开发技术, 注入蒸汽 1600t, 注氢气 2×10⁴Nm², 注降粘剂 15 t, 投产后, 峰值日产油 12t, 己生产 17 天, 平均日产油 10t, 含水 51.2%, 累 产油 176t。原油价格 3620 元吨, 新增产值 63 万元, 新增利禄 21 万元, 增 收节支 7 万元。





应用证明

	124.713	AND 191						
项目名称	傳成层超频油油藏在效开发关键技术研究均应用							
应用单位	中国石油化工程设有限公司胜利组织分公司新作采油厂							
通讯地址	山东东曾由肉酒路救建大厦新春采油厂。257009							
应用成果起止时间	2010/01-2013 12							
	经济效益	i (万元)						
年 度	2011	201,2	2013					
新增产值(产量)	60456	129130	230956					
新增利税(纯收入)	33121	59330	103356					
年期改节支总额	33421	59950	104250					

生禄子凸起非风法田位于莲噶尔盆地西北缘, 油碱建设该(450-600m), 油碱建设该, (26-29℃); 油稠(油碱条件下原油整度为50000-96000mPas), 漏子超稠油; 油层薄, 油层有效厚度为2~7m, 油层平均厚度为5m, 采用常规热采技术开发效果差。

为改善开发效果,实现没薄层超频油绘藏的药效开发,在存风油用拌 601 中区、南区、 排 6 南区、排 601-20、排 612 等 5 个区块探索实施了 HDN8 开发技术,共应用 277 口水 甲并988 并次。

項目实施后,2011年增值14.3 万吨,原油价格为 5709 元吨;2012年增泊34.9 万吨, 原油价格为 3700 元吨;2013年增油 63.8 万吨,原油价格为 3620 元吨;2014年1-5 月 增油34.2 万吨,原油价格为 3620 元吨,截止目前,累计增值153.2 万吨,新增产值 480968 万元,新常利税195807 万元,增载节支197621 万元。



应用证明

项目名称	厚浅层超褐油油藏高放开发关键技术研究与应用							
应用单位	中国石油化工程份有限公司社利油回分公司新春采油厂							
通讯地址	山东东营市西网路633号陆建大厦新春采油厂, 257000							
应用成果悬止时间	2010.06-2012.12							
	经济效益	(方元)						
年 度	2010	2011	2012					
新增产值 (产量)	12887.1	35977, 3	24420.0					
新增利税(纯收入)	4747.1	16577.3	11220.0					
年增收节支总额	4960. 8	19970.0	12310.5					

春风油田縣 601 北区具有"浅、薄、低、稠"的特点,在开发中面俗以 下难点: (1) 地层温度下原油粘度高; (2) 储层埋藏浅,生产压差小; (3) 油 层厚皮薄, 地层能量低。

为实现该区的高效开发,从2010年6月开始,在排601兆区开始实施HDNS 开发技术。项目实施后,2010年实现增油3.7万吨;2011年实现增油9.7万 吨;2012年实现增油6.6万吨。累计增油20.0万吨,新增产值73284.4万元。 新增利税32544.4万元,增收节支37231.0万元。

同时,"春风油田排 601 浅层超频油 HDNS 热化学春吐开发试验" 被中石 化授予"高效开发试验项目"称号。



Cumulative oil production: 173.22×10⁴t

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(1) The oil recovery factor are affected by the steam temperature and injection rate.

(2) The viscosity of crude oil can be obviously reduced by the injection of viscosity depressant, and the higher volume of viscosity depressant, the higher oil recovery factor. The injection volume is 0.05PV of viscosity depressant.

(3) Through the injection nitrogen ,the recovery can be enhanced by profile control and pressurization. And when 0.05PV viscosity depressant and 0.8PV nitrogen were injected, the recovery rate was heightest ,which was 76.48%.

(4) Steam, nitrogen and viscosity depressant have good synergistic effect, the HDNS technology provides a solution for the effective exploitation of super heavy oil reservoirs which are hard to be developed in the ordinary way. The injection parameters of these three parameters can be optimized rationally according to economic indicators in field application.

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Thank you for your attention



